

## Example Sheet 5

### Suffix notation question

1. (a) Recall the definitions

$$e_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) \quad \text{and} \quad \omega_{ij} = \frac{1}{2} \left( \frac{\partial u_i}{\partial x_j} - \frac{\partial u_j}{\partial x_i} \right)$$

Show that the vorticity tensor  $\omega_{ij}$  is related to the vorticity vector  $\boldsymbol{\omega}$  by

$$\omega_k = -\epsilon_{kpq} \omega_{pq},$$

and hence show that

$$\omega_{ij} = -\frac{1}{2} \epsilon_{ijk} \omega_k.$$

- (b) We have defined the rate of energy dissipation by viscosity to be

$$\Phi = 2\mu \int_V e_{ij} e_{ij} dV.$$

Show that an equivalent expression is given by

$$\Phi = \mu \int_V |\boldsymbol{\omega}|^2 dV$$

where  $\boldsymbol{\omega}$  is the vorticity vector.

### Flows without inertia

2. Fluid flows steadily through a rigid cylindrical tube parallel to the  $z$ -axis with velocity

$$\mathbf{u} = (0, 0, w(x, y)),$$

in Cartesian co-ordinates, under a uniform pressure gradient  $G = -\partial p/\partial z$ .

- (a) Show that the Navier–Stokes equations are satisfied provided

$$\nabla^2 w = -G/\mu,$$

and state the appropriate boundary condition for the flow.

- (b) Suppose that the tube has an elliptical cross-section with semi-major axes  $a$  and  $b$ . Show that

$$w(x, y) = w_0 \left( 1 - \frac{x^2}{a^2} - \frac{y^2}{b^2} \right).$$

Find  $w_0$ , and also show that the volume flux  $Q$  (i.e. the volume of fluid passing any cross-section of the tube in unit time) is given by

$$Q = \frac{\pi a^3 b^3 G}{4(a^2 + b^2)\mu}.$$

3. Viscous fluid is confined in the space  $a < r < b$  between two infinitely long concentric coaxial rigid cylinders. The inner cylinder rotates with constant angular velocity  $\Omega$  about its axis, and the outer cylinder is at rest.

(a) Consider steady solutions of the Navier–Stokes equation in the form  $\mathbf{u} = (0, v(r), 0)$  in cylindrical polar co-ordinates  $(r, \theta, z)$ . Derive the second-order linear ODE that  $v(r)$  must satisfy, and state the relevant boundary conditions.

(b) Look for solutions to this ODE in the form  $v(r) \propto r^\alpha$  and hence find  $v(r)$ .

(c) Show that the torque (per unit length in  $z$ ) that must be applied to the inner cylinder to maintain the motion is

$$T \equiv - \int_0^{2\pi} 2\mu e_{r\theta} a^2 d\theta = \frac{4\pi\mu\Omega a^2 b^2}{b^2 - a^2}$$

where, for this flow,  $e_{r\theta} = \frac{r}{2} \frac{d}{dr} \left( \frac{v}{r} \right)$ .

4. Two infinite plates are hinged together at  $r = 0$  and open slowly over time with angular velocities  $\pm\Omega$ , so that their positions are  $\theta = \pm\Omega t$ . The space  $-\Omega t < \theta < \Omega t$ ,  $0 < r < \infty$  between them is filled with very viscous fluid.

(a) Write down the boundary conditions satisfied by  $u_r$  and  $u_\theta$  at  $\theta = \pm\Omega t$  and hence write down the boundary conditions for the streamfunction  $\psi(r, \theta, t)$ .

(b) Discuss the assumptions behind the derivation of the (approximate) slow flow equation

$$\left( \frac{\partial^2}{\partial r^2} + \frac{1}{r} \frac{\partial}{\partial r} + \frac{1}{r^2} \frac{\partial^2}{\partial \theta^2} \right)^2 \psi = 0.$$

Solve this equation by examining possible solutions of the form  $\psi = r^\alpha f(\theta)$ , and derive the solution

$$\psi = -\frac{\Omega r^2}{2} \left( \frac{\sin 2\theta - 2\theta \cos 2\Omega t}{\sin 2\Omega t - 2\Omega t \cos 2\Omega t} \right) \quad (1)$$

(c) Show that when  $2\Omega t = \pi/2$  the (instantaneous) streamlines are rectangular hyperbolas.

(d) Use (1) to make rough order-of-magnitude estimates of the terms  $\partial\mathbf{u}/\partial t$ ,  $\mathbf{u} \cdot \nabla\mathbf{u}$  and  $\nu\nabla^2\mathbf{u}$  and hence deduce that the slow flow approximation is only valid if

$$\frac{\Omega r^2}{\nu} \ll 1.$$

Discuss the validity of the solution (1) for small and large  $r$ .